# **Autoignition of Methane Mixtures:** The Effect of Hydrogen Peroxide

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The objective of this study was to estimate the efficiency of autoignition promotion for  $CH_4$  combustible mixtures by  $H_2O_2$ . This was accomplished by computing ignition delays for  $CH_4/O_2/Ar(N_2)$  mixtures for various compositions, additive concentrations, pressures, and temperatures. Ignition delay times for additive-free compositions were predicted in good agreement with available experimental data. A model demonstrates that replacing 5-10% (volumetric) of the fuel with  $H_2O_2$  shortens the ignition delay by over one order of magnitude for all conditions examined. The effect of promotion is particularly pronounced at temperatures T < 1500 K.

# Introduction

CONTROL of ignition processes by addition of promoters (additives reducing ignition delay time) to burn  $H_2$  or HC fuels efficiently in air is an increasingly interesting method for improving the performance of airbreathing propulsion systems. Compounds used as promoters are free radicals, nitrogen oxides, peroxides, and others such as  $SiH_4$ . In looking for suitable promoters one should consider not only effectiveness in a general sense (i.e., dependence on combustor pressure, temperature, and air/fuel mixture ratio), but also availability, cost, impact on atmospheric chemistry (e.g., the ozone layer), toxicity, and many other technology-related factors.

The role played by nitrogen oxides introduced into a hydrogen-air system has been studied in detail by Laster and Sojka, and Baranovskii et al. A study of the effect of adding  $H_2O_2$  to a supersonic  $H_2$ /air diffusion flame has been reported elsewhere.

Since among HC fuels methane is most attractive because of its relatively large specific impulse and good cryogenic cooling properties for sustained hypersonic flight, but it is also least reactive, the selection of efficient promoters for methane may become an important issue, especially for wind-tunnel testing. Typical ignition delay for stoichiometric methane/air may reach upwards of  $\mathbb{O}(10^{-2}-10^{-1})$  s at combustor  $T_c \sim 1100$  K and  $P_c \sim 1$  atm, thereby preventing stable flame anchoring unless a strong recirculating region is maintained at the expense of large pressure drop. Ignition itself may be an even more serious problem because of the narrow flammability limits of methane.

Systematic data on the effect of stable additives, higher HC fuels, and free radicals on methane ignition are summarized by Zamansky and Borisov. Ramohalli et al. boserved experimentally the improved flame stability for fuel lean  $CH_4$ /air mixtures with 3% injection of  $H_2O_2$  that suggests an important role of  $H_2O_2$  in the ignition process.

The purpose of this study is to investigate the effects of hydrogen peroxide  $H_2O_2$  as promoter on the ignition delay times for methane/air combustion.  $CH_4/O_2/Ar$  mixtures were studied and simulated numerically, since reliable experimental data on ignition delay times for these (promoters-free) mixtures are available. <sup>6,7</sup> Lifshitz et al. <sup>6</sup> also considered  $H_2$  and  $C_3H_8$  as additives. Then  $CH_4/air$  mixtures were simulated. Numerical results indicate that moderate  $H_2O_2$  addition reduces delay times by about one order of magnitude in the temperature range of 1525-2025 K and the pressure range of 2.55-13.01 atm of the experiments. <sup>6</sup> Substantial reduction of ignition delay time was obtained also for stoichiometric and non-stoichiometric  $CH_4/air$  mixtures at conditions of interest for designers of supersonic combustion chambers operation.

# **Model Description**

The ignition delay time is related to a latent period in the combustion process of a premixed mixture, when the temperature stays nearly constant. During this period, however, the mixture components may experience essential changes. In this study a computer model was used to calculate the mixture parameters as a function of time, and the ignition delay time was defined as the time at which the temperature gradient picks up (point of inflection of the temperature vs time profile).

The detailed reaction mechanism of methane oxidation for a set of 23 species ( $H_2$ ,  $O_2$ , OH, H,  $H_2O$ , O,  $H_2O_2$ ,  $HO_2$ , CH<sub>4</sub>, CO, CO<sub>2</sub>, HCO, CH<sub>2</sub>O, CH<sub>3</sub>, CH<sub>2</sub>, CH, Ar or N<sub>2</sub>, N, NO, N<sub>2</sub>O, NO<sub>2</sub>, HNO) was generated in an automatic way from the C/H/O/N chemical system database employed. Each of  $N_r$  elementary chemical reactions involving  $N_s$  species is in the general form

$$\sum_{s=1}^{N_s} \nu'_{sr} X_s \stackrel{k'_f}{\rightleftharpoons} \sum_{s=1}^{N_s} \nu''_{sr} X_s, \qquad r = 1, N_r$$
 (1)

where  $X_s$  is the mole of s species,  $\nu'_{sr}$  and  $\nu''_{sr}$  are stoichiometric coefficients, and  $k'_f$  and  $k'_b$  are the rate coefficients for the forward and backward stages of the r reaction and are cast in the generalized Arrhenius form:

$$k_f' = a_f' T^{\xi_f'} \exp(-E_{af}'/T)$$

$$k_b' = a_b' T^{\xi_b'} \exp(-E_{ab}'/T)$$
(2)

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Table 1 Reaction mechanism for CH<sub>4</sub>/O<sub>2</sub>/Ar mixtures<sup>a</sup>

Reaction Reaction	$a_f^r$	ζŗ	$E_{af}^{r}$
$1. \text{ CH}_3 + \text{H} + M^b \Rightarrow \text{CH}_4 + M$	$8.00 \times 10^{26}$	-3.00	- <i>u</i> /0
2. $CH_4 + O_2 = CH_3 + HO_2$	$7.90 \times 10^{13}$	0.00	56,000
$3. CH_4 + H \Rightarrow CH_3 + H_2$	$2.20 \times 10^{04}$	3.00	8,750
4. $CH_4 + OH = CH_3 + H_2O$	$1.60 \times 10^{6}$	2.10	2,460
$5. \text{ CH}_4 + \text{O} \Rightarrow \text{CH}_3 + \text{OH}$	$1.02 \times 10^{09}$	1.50	8,604
6. $CH_4 + HO_2 \Rightarrow CH_3 + H_2O_2$	$1.80 \times 10^{11}$	0.00	18,700
7. $CH_3 + O_2 = CH_2O + OH$ 8. $CH_3 + O = CH_2O + H$	$2.50 \times 10^{11}$ $8.00 \times 10^{13}$	0.0 0.0	9,000 0
9. $CH_3 + O = CH_2O + H_2O$	$7.50 \times 10^{06}$	2.0	5,000
10. $CH_3 + H = CH_2 + H_2$	$9.00 \times 10^{13}$	0.0	15,100
$11. CH_2 + H \Rightarrow CH + H_2$	$1.00 \times 10^{18}$	-1.56	Ô
12. $CH_2 + OH = CH + H_2O$	$1.13 \times 10^{07}$	2.0	3,000
13. $CH_2 + OH = CH_2O + H$	$2.50 \times 10^{13}$	0.0	0
14. CH + $O_2 = HCO + O$	$3.30 \times 10^{13}$ $5.70 \times 10^{13}$	0.0	0
15. CH + O ≠ CO + H 16. CH + OH ≠ HCO + H	$3.00 \times 10^{13}$	0.0 0.0	0
17. $CH + CO_2 = HCO + CO$	$3.40 \times 10^{12}$	0.0	690
18. CH + $H_2O = CH_2O + H$	$1.17 \times 10^{15}$	-0.75	0
19. $CH_2 + CO_2 = CH_2O + CO$	$1.10 \times 10^{11}$	0.0	1,000
20. $CH_2 + O = CO + H + H$	$5.00 \times 10^{13}$	0.0	0
21. $CH_2 + O = CO + H_2$	$3.00 \times 10^{13}$	0.0	0
$22. CH_2 + O_2 \Rightarrow CO_2 + H + H$	$1.60 \times 10^{12} \\ 5.00 \times 10^{13}$	0.0	1,000
23. $CH_2 + O_2 = CH_2O + O$ 24. $CH_2 + O_2 = CO_2 + H_2$	$6.90 \times 10^{11}$	0.0 0.0	9,000 500
25. $CH_2 + O_2 = CO_2 + H_2O$	$1.90 \times 10^{10}$	0.0	-1,000
26. $CH_2 + O_2 = CO + OH + H$	$8.60 \times 10^{10}$	0.0	-500
27. $CH_2 + O_2 \Rightarrow HCO + OH$	$4.30 \times 10^{10}$	0.0	-500
28. CH2O + OH = HCO + H2O	$3.43 \times 10^{09}$	1.18	447
$29. \text{ CH}_2\text{O} + \text{H} \Rightarrow \text{HCO} + \text{H}_2$	$2.19 \times 10^{08}$	1.77	3,000
30. $CH_2O + M = HCO + H + M$	$3.31 \times 10^{16}$	0.0	81,000
31. $CH_2O + O \rightleftharpoons HCO + OH$ 32. $HCO + OH \rightleftharpoons H_2O + CO$	$1.80 \times 10^{13}$ $1.00 \times 10^{14}$	0.0 0.0	3,080 0
33. $HCO + M = H + CO + M$	$2.50 \times 10^{14}$	0.0	16,802
34. $HCO + H = CO + H_2$	$1.19 \times 10^{13}$	0.25	0
35. $HCO + O \Rightarrow CO + OH$	$3.00 \times 10^{13}$	0.0	0
$36. HCO + O = CO_2 + H$	$3.00 \times 10^{13}$	0.0	0
37. $HCO + O_2 \Rightarrow HO_2 + CO$	$3.30 \times 10^{13}$	-0.40	0
38. $CO + O + M_3^b = CO_2 + M_3$	$6.17 \times 10^{14}$ $1.51 \times 10^{07}$	0.0	3,000 758
39. $CO + OH = CO_2 + H$ 40. $CO + O_2 = CO_2 + O$	$1.60 \times 10^{13}$	1.30 0.0	41,000
$41. \text{ HO}_2 + \text{CO} = \text{CO}_2 + \text{OH}$	$5.80 \times 10^{13}$	0.0	22,934
$42. \text{ CH}_2 + \text{O}_2 \Rightarrow \text{CO} + \text{OH} + \text{H}$	$3.00 \times 10^{13}$	0.0	0
$43. \text{ CH}_2 + \text{H}_2 \Rightarrow \text{CH}_3 + \text{H}$	$7.00 \times 10^{13}$	0.0	. 0
$44. \text{ CH}_2 + \text{OH} = \text{CH}_2\text{O} + \text{H}$	$3.00 \times 10^{13}$	0.0	0
$45. H_2 + O_2 = OH + OH$	$1.70 \times 10^{13}$	0.0	47,780
46. $H_2 + OH = H_2O + H$ 47. $O + OH = O_2 + H$	$1.17 \times 10^{09}$ $4.00 \times 10^{14}$	1.30 -0.50	3,626 0
$48. O + H_2 = OH + H$	$5.06 \times 10^{04}$	2.67	6,290
49. H + O <sub>2</sub> + $M_2^b$ = HO <sub>2</sub> + $M_2$	$3.61 \times 10^{17}$	-0.72	0
$50. OH + HO_2 = H_2O + O_2$	$7.50 \times 10^{12}$	0.0	0
$51. H + HO_2 = OH + OH$	$1.40 \times 10^{14}$	0.0	1,073
$52. O + HO_2 = O_2 + OH$	$1.40 \times 10^{13}$	0.0	1,073
53. OH + OH = O + $H_2O$	$6.00 \times 10^{08}$	1.3	0
54. $H + H + M_1^b = H_2 + M_1$ 55. $H + H + H_2 = H_2 + H_2$	$1.00 \times 10^{18}$ $9.20 \times 10^{16}$	-1.0 -0.6	0
56. $H + H + H_2O = H_2 + H_2O$	$6.00 \times 10^{19}$	-1.25	. 0
57. $H + H + CO_2 = H_2 + CO_2$	$5.49 \times 10^{20}$	-2.0	Ö
$58. H + OH + M = H_2O + M$	$1.60 \times 10^{22}$	-2.0	0
59. H + O + M = OH + M	$6.20 \times 10^{16}$	-0.6	0
$60. O + O + M \Rightarrow O_2 + M$	$1.89 \times 10^{13}$	0.0	-1,788
61. H + HO <sub>2</sub> $\Rightarrow$ H <sub>2</sub> + O <sub>2</sub>	$1.25 \times 10^{13} \\ 2.00 \times 10^{12}$	0.0	0
62. $HO_2 + HO_2 = H_2O_2 + O_2$ 63. $H_2O_2 + M = OH + OH + M$	$1.30 \times 10^{17}$	0.0 0.0	0 45,500
64. $H_2O_2 + H = HO_2 + H_2$	$1.60 \times 10^{12}$	0.0	3,800
65. $H_2O_2 + OH = H_2O + HO_2$	$1.0 \times 10^{13}$	0.0	1,800
66. H + $HO_2 = O + H_2O$	$3.10 \times 10^{10}$	0.0	3,590
$67. O + OH + M = HO_2 + M$	$1.0 \times 10^{16}$	0.0	0
$68. \ H_2O_2 + H = H_2O + OH$	$1.00 \times 10^{13}$	0.0	3,590
69. $H_2O_2 + O = H_2O + O_2$	$8.40 \times 10^{11}$ $2.00 \times 10^{13}$	0.0 0.0	4,260 5,900
$70. H_2O_2 + O = OH + HO_2$			

 $<sup>^{</sup>a}$ Units are moles, cubic centimeters, seconds, Kelvins, and calories/mole.  $^{b}$ Third body concentrations  $M_{i}$  and the chaperon efficiencies were those of Miller and Bowman database.

Reaction rate parameters a',  $\zeta'$ , and  $E'_a$ , listed in Table 1, are taken mainly from Miller and Bowman. The parameters for the last two reactions in this table were taken from Wu et al. The additional methyl-consuming reaction

$$CH_3 + O_2 = CH_2O + OH$$

which was not included in the compilation is assumed to be important. The kinetics of this reaction derived from Tsuboi and Wagner are proven to be necessary to reproduce the ignition delay times measured in shock-tube experiments. To reproduce correctly the equilibrium limit, the Arrhenius parameters for the backward reactions in Eqs. (2) were calculated with the help of a linear regression analysis to obtain the best-fit values of  $k_b^r = k_f^r/K_c^r$ , where  $K_c^r$  is the equilibrium constant for the r reaction. The equilibrium constants and species properties were calculated with the help of the well-known NASA polynomials. 12

The high-temperature oxidation mechanism was not tuned for any particular composition, temperature, or pressure conditions, and does not contain  $C_2$  chemistry.<sup>13</sup> The initial step of the ignition process is the fuel decomposition reaction

$$CH_4 + M \Rightarrow CH_3 + H + M \tag{3}$$

whose pressure-dependent falloff nature has been neglected. The N-O reactions used to simulate ignition processes in  $CH_4$ /air mixtures are listed in Table 2.

The mathematical zero-dimensional model that describes the time evolution of homogeneous mixtures parameters, in an adiabatic, constant pressure environment simulating that of an aerocombustor, is formulated as an initial value problem for the system of ordinary differential equations (ODEs)<sup>14</sup>

$$\rho \frac{dy_i}{dt} = f_i(c) = W_i \sum_{r=1}^{N_r} (\nu_{ir}'' - \nu_{ir}') \dot{\omega}_r$$

$$(y_i)_{i=0} = y_i^0, \qquad i = 1, N_s$$
(4)

supplemented by the two algebraic constraints

$$H(t) = \sum_{i=1}^{N_s} y_i h_i(T) = \text{const}$$

$$P(t) = R_0 T \sum_{i=1}^{N_s} c_i = \text{const}$$
(5)

Here,  $c_i = \rho_i/W_i$  and  $y_i$  are the numbers of moles in cm<sup>3</sup> and mass fractions, respectively, t is the time, H and  $h_i(T)$  are total enthalphy and enthalphies of i species, respectively,  $W_i$  and  $\rho_i$ 

Table 2 N-O Reactions

Reaction	$a_f^r$	$\zeta_f^r$	$E_{af}^{r}$
$1. CO_2 + N = NO + CO$	$1.90 \times 10^{11}$	0.00	3,400
2. $HO_2 + NO \Rightarrow NO_2 + OH$	$2.11 \times 10^{12}$	0.00	-479
3. $NO_2 + H \Rightarrow NO + OH$	$3.50 \times 10^{14}$	0.00	1,500
$4. NO_2 + O \Rightarrow NO + O_2$	$1.00 \times 10^{13}$	0.00	600
5. $NO_2 + M \Rightarrow NO + O + M$	$1.10 \times 10^{16}$	0.00	66,000
6. $N_2O + OH \Rightarrow N_2 + HO_2$	$2.00 \times 10^{12}$	0.00	10,000
7. $N_2O + H = N_2 + OH$	$7.60 \times 10^{13}$	0.00	15,200
8. $N_2O + M = N_2 + O + M$	$1.60 \times 10^{14}$	0.00	51,600
$9. N_2O + O \Rightarrow N_2 + O_2$	$1.00 \times 10^{14}$	0.00	28,200
10. $N_2O + O \Rightarrow NO + NO$	$1.00 \times 10^{14}$	0.00	28,200
11. HNO + $M \Rightarrow$ H + NO + $M$	$1.50 \times 10^{16}$	0.00	48,680
12. HNO + OH $\Rightarrow$ NO + H <sub>2</sub> O	$3.60 \times 10^{13}$	0.00	0
13. HNO + H $\rightleftharpoons$ H <sub>2</sub> + NO	$5.00 \times 10^{12}$	0.00	0
$14. N + NO \Rightarrow N_2 + O$	$3.27 \times 10^{12}$	0.30	0
15. $N + O_2 = NO + O$	$6.40 \times 10^{09}$	1.00	6,280
16. N + OH = NO + H	$3.80 \times 10^{13}$	0.00	0

<sup>&</sup>lt;sup>a</sup>Units are moles, cubic centimeters, seconds, Kelvins, and calories/mole.

are the *i* species molecular mass and density, T is the temperature, P is the pressure,  $R_0$  is the universal gas constant, and the variable  $\omega_r$  is the rate of progress of the rth reaction defined in terms of Arrhenius kinetics.

The steady state in such calculations corresponds to the equilibrium state. Since the time required to reach equilibrium generally exceeds the characteristic times associated with the most rapid reactions by several orders of magnitudes, the initial value problem for the so-called stiff ODEs [Eq. (4)] must be solved by appropriate methods. To integrate numerically the

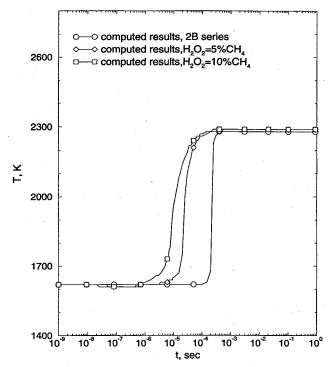


Fig. 1 Time history for temperature used to define ignition delay time

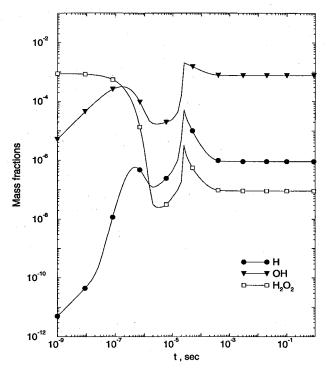


Fig. 2 Time history for radicals H and OH showing two maxima (equivalence ratio = 0.5, T = 1617 K, P = 8.6 atm,  $H_2O_2 = 5\%$  CH<sub>4</sub>).

system [Eq. (4)], a linear, multistep method developed by Gear was used in the Kinetics code. The Kinetics code uses computer-aided generation of the reaction mechanism, selects rate coefficients and species thermal properties by preprocessing the specialized databases, generates the numerical solution with an automatic choice of time steps and order of integration, and performs local sensitivity analysis based on the decomposed direct method.<sup>15</sup>

#### **Results and Discussion**

## Comparison with Experiments

The ignition delays were at first computed and compared with experimental data for the additive-free  $CH_4/O_2/Ar$  mixtures. Such a comparison was performed to assess the accuracy of the kinetic mechanism in the absence of additives. Some temperature vs time histories used to define the ignition delay times are plotted in Fig. 1. It is interesting to note that when  $H_2O_2$  is added, H and OH radicals exhibit two maxima (see Fig. 2): the first one is caused by  $H_2O_2$  decomposition, and the second is related to combustion of the main fuel. At

Table 3 Composition of test gas mixtures (in volume %) and experimental 6 conditions

1C     3.5     7     89.5     —     1752     10.92       —     —     —     1805     10.92       —     —     1832     11.42       —     —     1587     8.42       2B     2     8     90     —     1617     8.66       —     —     —     1749     9.44       —     —     —     1677     9.33       4A     3.5     7     89.427     H <sub>2</sub> 0.073     1722     10.44       —     —     —     1760     10.53       —     —     —     1698     10.53							
2B 2 8 90 — 1617 8.64 — — — — 1712 9.44 4A 3.5 7 89.427 H <sub>2</sub> 0.073 1722 10.45 — — — — 1698 10.55	Series	CH₄	$O_2$	Ar	Additive	<i>T</i> , K	P, atm
2B 2 8 90 — 1617 8.66 — — — — 1749 9.4' — — — — 1712 9.4' — — — 1677 9.3' 4A 3.5 7 89.427 H <sub>2</sub> 0.073 1722 10.4' — — — 1698 10.5'	1C	3.5	7	89.5		1752	10.95
2B 2 8 90 — 1617 8.6 — — — — 1749 9.4 — — — — 1712 9.4 — — — 1677 9.3 4A 3.5 7 89.427 H <sub>2</sub> 0.073 1722 10.4 — — — 1760 10.5 — — — 1698 10.5						1805	10.97
2B 2 8 90 — 1617 8.60 — — — — 1749 9.4 — — — 1712 9.4 — — — 1677 9.3 4A 3.5 7 89.427 H <sub>2</sub> 0.073 1722 10.4 — — — 1760 10.5 — — — 1698 10.5				<del></del>		1832	11.43
						1587	8.43
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	2B	2	8	90		1617	8.60
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1760 10.5: 1698 10.5:						1677	9.33
<u> </u>	4A	3.5	7	89.427	$H_2 0.073$	1722	10.47
						1760	10.55
				<del></del>		1698	10.53
						1630	10.00

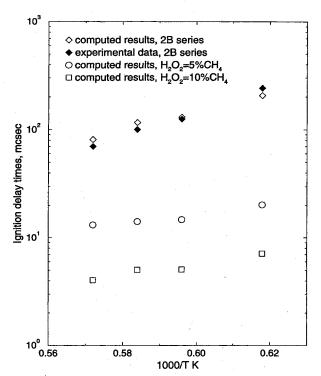


Fig. 3 Effect of  $H_2O_2$  on  $CH_4/O_2/Ar$  mixtures ignition delay times and comparison with experimental (additive-free) data (2B-series from Table 3).

the early stage of ignition  $H_2O_2$  is rapidly decomposed via the reaction

$$H_2O_2 + M = OH + OH + M \tag{6}$$

and thus  $H_2O_2$  serves as the major radical source. At later times, i.e., during radical pool formation because of chain

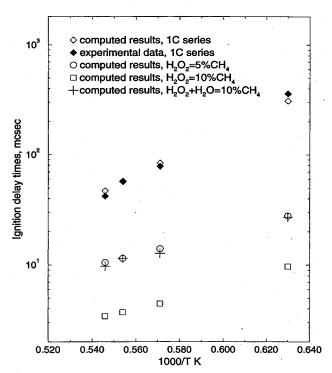


Fig. 4 Effect of  $\rm H_2O_2$  addition on  $\rm CH_4/O_2/Ar$  mixtures ignition delay times and comparison with experimental (additive-free) data (1C-series from Table 3).

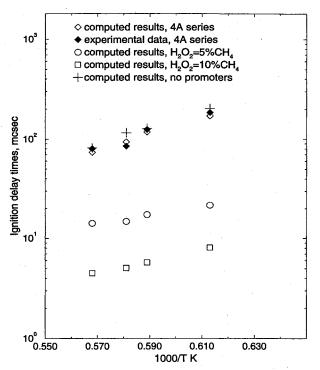


Fig. 5 Computed ignition delay times and comparison with experimental data when  $H_2$  was used as additive (4A-series from Table 3).

branching, some  $H_2O_2$  is again formed through a propagation step

$$CH_4 + HO_2 \Rightarrow CH_3 + H_2O_2 \tag{7}$$

and also from the partial recombination of OH. The methyl,  $CH_3$ , and the hydrogen peroxy,  $HO_2$ , radicals are the most abundant in the radical pool. The oxidation of  $CH_3$  proceeds via the sequence:  $CH_3 \rightarrow CH_2O \rightarrow HCO \rightarrow CO$ . The radical  $HO_2$  is almost exclusively produced through the stages

$$H + O_2 + M \Rightarrow HO_2 + M$$
  
 $H_2O_2 + O_2 \Rightarrow HO_2 + HO_2$ 
(8)

Compared to the first reaction, the second in Eq. (8) becomes important only if initial  $H_2O_2$  is large. Therefore two independent paths forming  $HO_2$  [and then  $H_2O_2$  through Eq. (7)] exist. The first reaction of Eq. (8) depends on H, which peaks simultaneously with OH:

$$H_2 + OH \Rightarrow H + H_2O \tag{9}$$

Thus, the H and OH maxima become related. When  $H_2O_2$  is added, therefore, the conventional ignition delay time definition based on H concentration maximum used by Meyer and Oppenheim<sup>16</sup> is no longer suitable. The criterium for the ignition delay time used by Schott and Kinsey,<sup>17</sup> [OH] =  $10^{-9}$  mole/cm<sup>3</sup>, also does not work here because almost immediately OH concentrations exceeds this level by two orders of magnitude. This is why the definition of ignition delay time as that corresponding to the point of inflection of the temperature pro-

Table 4 Composition of test gas mixtures (in volume %) and experimental<sup>7,19</sup> conditions

			_			
Series	CH <sub>4</sub>	O <sub>2</sub>	Ar	Air	<i>T</i> , K	P, atm
A	7.7	15.4	76.9		1476-1900	11.22-15.13
A1	: 2	20	78		1470-1850	
A2	2			98	1450-1740	
A4	4		. —	96	1560-1700	

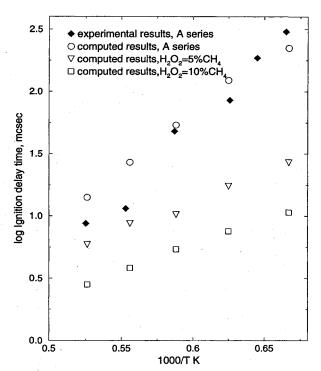


Fig. 6 Ignition delay times for A-series from Table 4.

file is employed in this study. In fact, the time so defined is well correlated to the second maximum of H concentration vs time profile and with the point at which the largest sensitivity coefficients occur.

The satisfactory agreement with the experimental data for selected series<sup>6</sup> (see Table 3): 1C (stoichiometric), 2B (lean, equivalence ratio equal 0.5), and 4A (stoichiometric, with  $H_2$  as additive) are demonstrated in Figs. 3–5. The results for  $CH_4/O_2/Ar$  mixtures when hydrogen peroxide is added (addition is reported as % volumetric) show an essentially monotonous reduction of ignition delay times. As  $H_2O_2$  is practically available as aqueous solutions of various strengths, the efficiency of a 50% solution was also investigated. From the

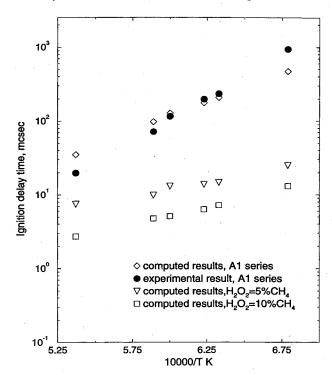


Fig. 7 Ignition delay times for A1-series from Table 4.

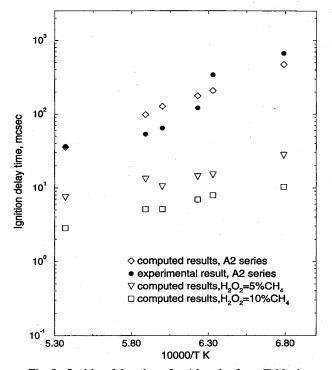


Fig. 8 Ignition delay times for A2-series from Table 4.

results in Fig. 4, it follows that only  $\rm H_2O_2$  may be considered as a chemically active agent reducing ignition delay, the influence of the associated  $\rm H_2O$  initial concentration being negligible. Hydrogen peroxide proved to be more effective than, for example,  $\rm H_2$ , as shown in Fig. 5. This is of importance, because Taguchi et al. <sup>18</sup> used a methane-hydrogen mixture as fuel and injected it into a high-enthalpy supersonic airstream. Therefore ignition delays for series 4A were calculated also for additive-free conditions and compared with those including  $\rm H_2$ . Hydrogen cannot be considered, strictly speaking, as a pro-

was found to be rather weak and was explained on a pure thermal basis, i.e., by increasing heat release and final products temperature, while  $H_2O_2$  acts mainly as a gas catalyst, i.e., the mixture composition and temperature at final equilibrium remain unchanged. From these results we can conclude that moderate  $H_2O_2$  addition reduces delay times by over one order of magnitude in the temperature range of 1525-2025 K and in the pressure range of 2.55-13.01 atm of the experiments. The other experimental series used to compare theoretical and

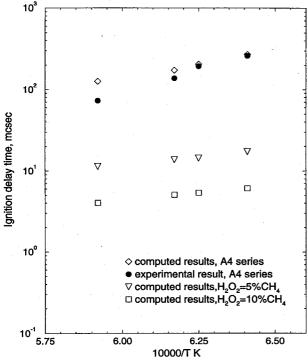


Fig. 9 Ignition delay times for A4-series from Table 4.

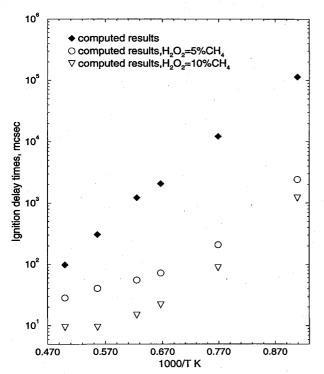
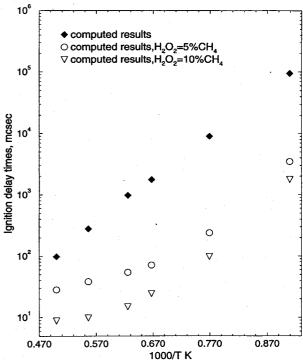


Fig. 10 Computational modeling (no experimental data) of the effect of  $\rm H_2O_2$  on  $\rm CH_4/Air$  mixtures ignition delay times (P=1 atm, equivalence ratio = 1).



moter, but rather an easily ignitable fuel. Its overall influence

Fig. 11 Effect of  $H_2O_2$  on  $CH_4$ /air mixtures ignition delay times (P=1 atm, equivalence ratio = 0.5).

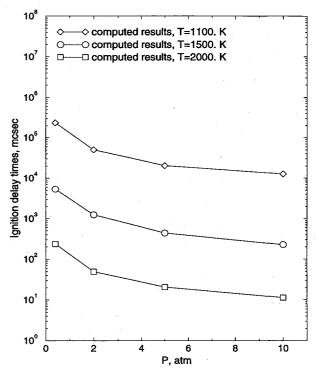


Fig. 12 Effect of pressure on CH<sub>4</sub>/air mixtures ignition delay time (additive-free mixtures, equivalence ratio = 1).

experimental data are presented in Table 4.7,19 The series A19 refers to stoichiometric CH<sub>4</sub>/O<sub>2</sub>/Ar mixtures with a reduced amount of diluent. The series A17 represents a fuel lean mixture with synthetic air  $(O_2/Ar = 20/80)$ , and series A2-A4<sup>7</sup> correspond to fuel lean mixtures with raw laboratory air. To investigate the effect of the promoter addition for these cases, 5-10% of fuel was again substituted by H<sub>2</sub>O<sub>2</sub>. Not all initial conditions were explicitly stated in the information provided<sup>7,19</sup> for each experiment. In the experimental data by Burcat et al. 19 the pressure and temperature range and the condition of constant density were specified, whereas in those by Eubank et al.  $^{7}$  the total density (3.0  $\times$  10<sup>-5</sup> mol/cm<sup>3</sup>) and the temperature range were specified. Therefore, the parameters not explicitly specified were calculated through the thermal equation of state [Eq. (5)]. The results of calculations and comparison with experiments are plotted in Figs. 6-9. They again indicate reasonable agreement with the experimental data and the shortening of ignition delays when H<sub>2</sub>O<sub>2</sub> was added.

#### Effect of H<sub>2</sub>O<sub>2</sub> Addition

The validation of predictions by means of the experimental data implies that the chemical mechanism and its numerical solution should be considered sufficiently reliable to predict new results. Examples of such theoretical predictions, still using the scheme of Tables 1 and 2, refer to autoignition for CH<sub>4</sub>/air stoichiometric (Fig. 10) and fuel lean (equivalence ratio equal 0.5, Fig. 11) mixtures at atmospheric pressure, for which experimental data are missing. The results for fuel-rich (equivalence ratio equal 2.0) mixtures are qualitatively the same and are not reported. These conditions would be of interest for practical supersonic combustion ramjets (SCRJ) and lean mixture gas-turbine applications, respectively. In this last application the difficulties associated with premixed, lean operation are well known: rough operation, vibrations, noise, and relighting problems. The positive effect of H<sub>2</sub>O<sub>2</sub> is well pronounced, especially for low temperatures (T < 1500 K). The effect of pressure on ignition delay time has been also investigated. Predictions (Fig. 12) show that ignition delay time regularly decreases as pressure increases, in the range P =1100-2000 K, and this behavior is confirmed in the presence of  $H_2O_2$  (Figs. 13-15). The data for temperatures T < 1300 K

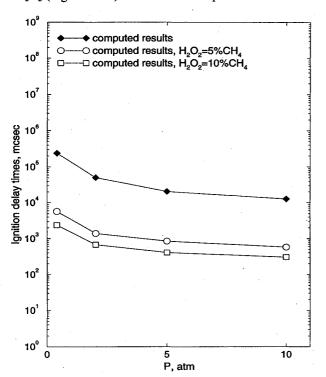


Fig. 13 Effect of pressure on additive-free and additive-added  $CH_4$ /air ignition delay time (To = 1100 K, equivalence ratio = 1).

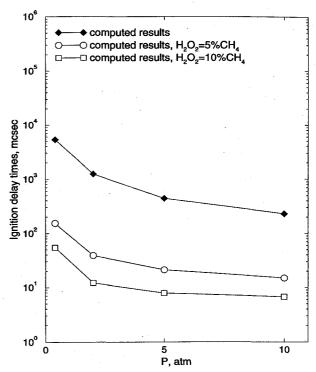


Fig. 14 Effect of pressure on additive-free and additive-added  $CH_4$ /air ignition delay time (To = 1500 K, equivalence ratio = 1).

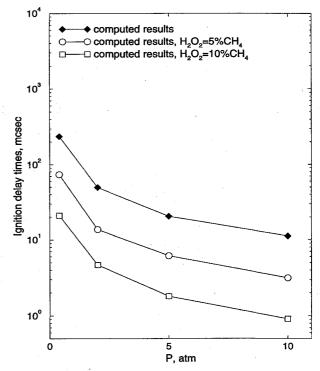


Fig. 15 Effect of pressure on additive-free and additive-added  $CH_4$ /air ignition delay time (To = 2000 K, equivalence ratio = 1).

should be considered only as estimates, since at such temperatures C<sub>2</sub> chemistry may become important.

To explain the effect of  $H_2O_2$  on oxidation process acceleration, it is necessary to consider the dominant role of stage Eq. (6) in the reactions (6–9), in accordance with Chen et al. To support this assumption, local sensitivity analysis based on the decomposed direct method was performed. The sensitivities of temperature to small changes in reaction rates were calculated via  $s_j = \partial T/\partial k_j$  (j is the reaction index), and the 12 most important reactions are listed in Table 5 at two particular

Table 5 Absolute reaction sensitivities\*

Reaction	$t = 0.5 \mu s$	$t = 44.5 \ \mu s$
$H_2O_2 + M \rightleftharpoons OH + OH + M$	7.72	36.5
$CH_3 + OH \Rightarrow CH_2 + H_2O$	3.90	574
$CH_3 + H = CH_2 + H_2$	2.81	-1040
$CH_4 + OH \Rightarrow CH_3 + H_2O$	-2.71	304
$CH_3 + O \Rightarrow CH_2O + H$	1.55	-656
$CH_4 + OH = CH_3 + H_2O$	-1.41	-764
$CH_3 + O_2 = CH_2O + OH$	1.33	3070
$H + H + M \Rightarrow H_2 + M$	1.02	-0.327
$CH_3 + H + M \Rightarrow CH_4 + M$	0.86	1810
$CH_4 + O \Rightarrow CH_3 + OH$	-0.77	358
$O + H_2 = OH + H$	0.745	3720
$CH_2O + H \Rightarrow HCO + H_2$	0.662	532

<sup>a</sup>Case 2 of 1C series,  $^6$  H<sub>2</sub>O<sub>2</sub> = 5% CH<sub>4</sub>.

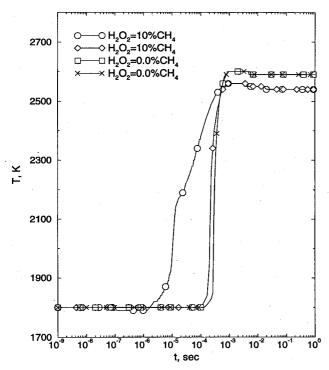


Fig. 16 Temperature vs time profiles for explanation of the mechanism of ignition acceleration. For regimes labeled by  $\Diamond$  and  $\times$  the reaction (6) is suppressed.

times. The key role of reaction (6) is shown during the initial phase of the ignition period ( $t \le 0.5 \ \mu s$ ). A numerical experiment was also performed to further validate this conclusion and some of its results are presented in Fig. 16. The temperature vs time curve for the fuel lean mixture ( $T_0 = 1800 \ K$ ,  $P_0 = 1 \ atm$ , equivalence ratio = 0.5) with 10% of  $H_2O_2$  added is labeled by  $\circ$ . The temperature profile obtained for the same conditions, but with the reaction (6) suppressed is labeled by  $\diamond$ . The profiles labeled by  $\Box$  and  $\times$  are the correspondent additive-free mixture cases. The nearly coincident last three temperature profiles illustrate the dominance of reaction (6) in the mechanism of acceleration for nonzero initial concentration of  $H_2O_2$ . This explanation was also found true by repeating sensitivity analysis and checking the effects of suppressing reaction (6), for stoichiometric and rich mixtures.

The practical advantage of  $\rm H_2O_2$  as a free radical promoter is its stability, until inside the high temperature zone. It can be quickly transported into the flame and after rapid decomposition it releases free radicals at the key location of the ignition process.

#### **Conclusions**

Methane autoignition promotion by hydrogen peroxide has been predicted using a computer model, emphasizing the detailed oxidation chemistry for  $CH_4/O_2/Ar$  and  $CH_4/air$  mixtures. Numerical results are in good agreement with experimental data for all promoter-free compositions available in the literature. Hydrogen peroxide at concentrations below 10% (volumetric) significantly reduces the ignition delay for  $CH_4/O_2/Ar$  mixtures in the pressure range of 2.55–13.01 atm in the temperature range of 1525–2025 K, and for  $CH_4/air$  mixtures in the pressure range of 0.4–10 atm and in the temperature range of 1100–2000 K, acting mainly as a gas catalyst in chain-branching reactions.

The mechanism of ignition acceleration is attributed to the dominant role of reaction (6) for all mixtures with nonzero initial concentrations of  $H_2O_2$ . Applications of those findings may include methane-fueled cruise SCRJ as well as advanced conventional ramjet and gas turbine combustors based on lean premixed combustion.

## Acknowledgment

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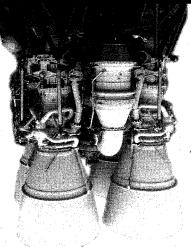
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